Advances in boiling simulations using interface tracking methods and microscale modeling



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THE NEED FOR PREDICTIVE SIMULATIONS



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Bubble radius reaches mm within ms

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MICROLAYER FORMS, THEN EVAPORATES



H. Kim, J. Buongiorno, Detection of Liquid-Vapor- Solid Triple Contact Line in Two-Phase Heat Transfer Phenomena Using High-Speed Infra-Red Thermometry, Int. J. Multiphase Flow, 37, 166-172 (2011)

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⁺V. K. Dhir, Simulation of boiling how far we have come!, ECI International Conference on Boiling Heat Transfer, Florianopolis-SC-Brazil, 3-7 May 2009.

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[¶]A. Guion, D. Langewisch, J. Buongiorno, Dynamics of the liquid microlayer underneath a vapor bubble growing at a heated wall, Proceedings of the ASME Summer Heat Transfer Conference HT2013 July 14-19, 2013, Minneapolis, MN, USA.

$$\frac{\partial_t \delta}{\partial_t \delta} = -\frac{k_l}{\rho_f h_{fg}} \frac{T_w - T_{sat}}{\delta}$$

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► Complements existing literature

- 1. static models^{*†‡}
- 2. evaporation models[§]

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MODEL CAPTURES CONSISTENT DYNAMICS







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▶ Gap in literature

- 1. limited experimental data (see length and time scales)
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▶ Need for simulations of inertial bubble growth

- 1. model mass transfer with an overpressure at interface
- 2. compare simulation with reference growth[†]
- 3. inform dynamics of microlayer formation

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DETERMINE INITIAL SHAPE, USING GERRIS

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REFERENCE GROWTH RATE: NO WALL (∞ LIQUID)

Rayleigh solution:



 $^{{}^{*}}$ The equivalent radius can be found by matching the simulated bubble volume with a perfect hemisphere (half a sphere)





 $\delta = \mathbf{f} (\mu_v, \mu_l, \rho_v, \rho_l, \Delta P, \sigma, \theta, R_b, r)$



$$\delta = \mathbf{f} \left(\begin{array}{c} \mu_{v}, \mu_{l}, \rho_{v}, \rho_{l}, \Delta P, \sigma, \theta, R_{b}, r \end{array} \right)$$
$$U_{b} = \sqrt{\frac{2\Delta P}{3\rho_{l}}} \quad Re = \frac{\rho_{l}U_{b}R_{b}}{\mu_{l}} \quad Ca = \frac{\mu_{l}U_{b}}{\sigma}$$

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$$\delta = f \left(\begin{array}{l} \mu_{v}, \mu_{l}, \rho_{v}, \rho_{l}, \Delta P, \sigma, \theta, R_{b}, r \end{array} \right)$$
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$$\boxed{\frac{\delta}{R_{b}} = f \left(\frac{\mu_{v}}{\mu_{l}}, \frac{\rho_{v}}{\rho_{l}}, \frac{r}{R_{b}}, Re, Ca, \theta \right)}$$

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SIMULATION OF INERTIAL BUBBLE GROWTH (r,z) domain: $120\mu m \times 120\mu m$, cavity size $r_c = 10\mu m$

SIMULATION OF INERTIAL BUBBLE GROWTH (r,z) domain: $120\mu m \times 120\mu m$, cavity size $r_c = 10\mu m$ $P_{root} = 50$ kPa, Re ~ 200, Ca = 0.03, $\theta = 10^{\circ}$

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SIMULATED BUBBLE BECOMES HEMISPHERICAL $P_{root} = 50$ kPa, Re ~ 200, Ca = 0.03, $\theta = 10^{\circ}$



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SIMULATED GROWTH MATCHES REFERENCE $P_{root} = 50 \text{ kPa}, \text{ Re} \sim 200, \text{ Ca} = 0.03, \theta = 10^{\circ}$



SIMULATED MICROLAYER PROFILES

 $P_{root} = 50$ kPa, Re ~ 200, Ca = 0.03, $\theta = 10^{\circ}$



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- ▶ Simulations of inertial bubble growth
 - 1. model mass transfer with an overpressure at interface
 - 2. compare simulation with reference growth^{\dagger}

▶ Inform formation dynamics and initial shape

$$\frac{\delta}{R_b} = f\left(\frac{\mu_v}{\mu_l}, \frac{\rho_v}{\rho_l}, \frac{r}{R_b}, \frac{Re}{Re}, Ca, \theta\right)$$

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